The different renewable product generation via thermal processes suited to forestry raw materials

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South african context

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Wood and forestry raw materials

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Thermo-chemical processes

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Pyrolysis

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Mechanisms, renewable products, yields and parameters

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Toxicity

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Applications

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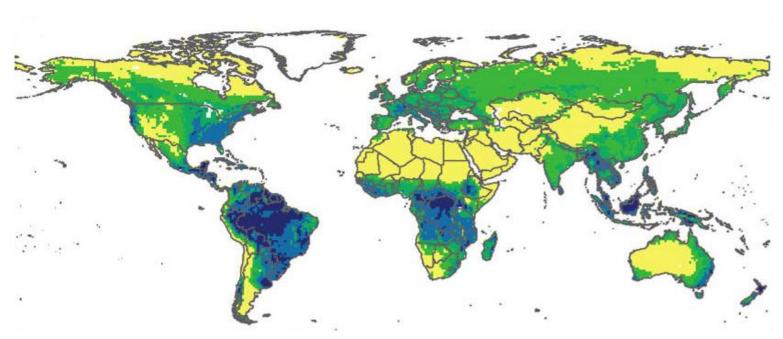
Commercial plants

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Keys-Challenges



Biomass potential



Natural Production (ton ha⁻¹ y⁻¹)

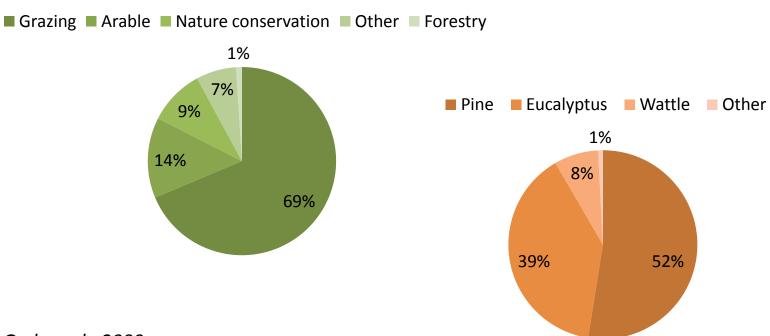
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- Large availability of natural resources
- Conversion of plant biomass is an attractive option



Why wood?

- One of the best renewable Carbon source (CO₂ sequestration)
- Wood resources in South Africa increasing, production of 16 m³/hectare while:
 - a decrease of plantation area from 1997
 - a small land use in South Africa

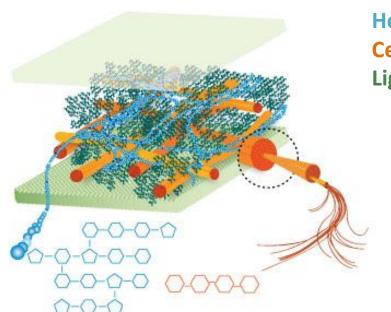




Godsmark, 2009

Why wood?

Lignocellulosic structure which leads to remarkable products



Hemicelluloses Cellulose Lignin

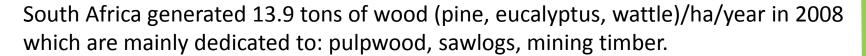
Woody biomass	Lignin (%)	Cellulose (%)	Hemicelluloses (%)	Reference
Pine	26.4	44.7	18.6	Hamelinck, 2005
Eucalyptus	27.7-25.9	49.5-57.3	13.1-16.8	Hamelinck, 2005; Kumar, 1992
Black Wattle	17.9-21.2	63.9	12.7	Lachke, 1988; Brown, 2007
Hardwood	16-25	40-50	35	Mohan, 2006
Softwood	23-33	40-50	28	Mohan, 2006
Pine bark	34	34	16	Arpiainen, 1989

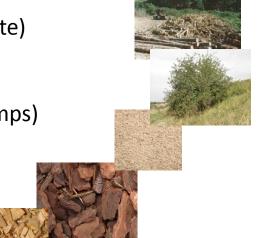


Which type of forestry materials?

Untreated wood wastes:

- Dry urban wastes (construction and demolition waste)
- Wood from plantations Poplar, Eucalyptus, Pine
- Logging residues
- Shrubs and wood residues (twigs, branches and stumps)
- Sawdust
- Bark
- Wood chips
- Damaged wood from plantation fires







Why Thermo-chemical processes?

- Carbon-neutral balance
- Lower emissions of NO_x, CO and hydrocarbons
- All the products from these processes can be used
- Improvement of efficiency of the energy conversion
- Production of sustainable energy sources
- Material cheap and readily available
- Relatively low capital investment
- Large range of potential products/feedstocks

Choice of conversion process depends upon the type and quantity of biomass feedstock, the desired form of the energy, end use requirements, environmental standards, economic conditions and project specific factors.



- **High moisture content** inhibits pyrolysis, leads to energy loss because used to evaporate water,
- Often low density, which makes them bulky and hard to store,
- Often **no homogeneous** form,
- Contain a fairly large amount of inorganic substances, which remains as ash,
- Environmental impact of pre-treatments used to separate or remove products.

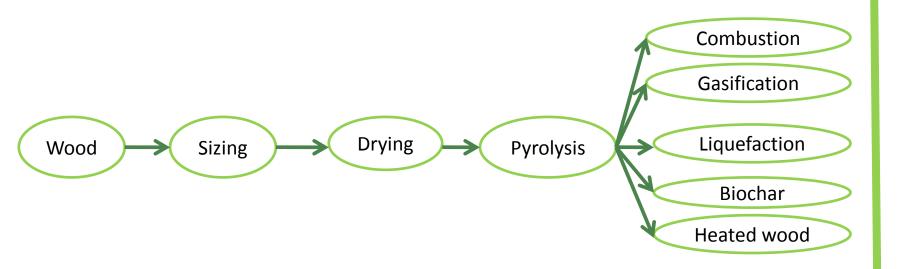


Thermo-chemical processes

Thermal Process	Temperature (°C)	Atmosphere	Products	Energy efficiency (%)
Combustion	> 900	O ₂ (air)	CO_2 + H_2O + N_2 + ashes to be treated	65
Pyrolysis	< 600	Inert gas or low pressure	Char + tars + gas, which proportions are related to the pyrolysis parameters	45
Gasification by Fast Pyrolysis	> 700	Inert gas or low pressure	Mainly gas (CO, H_2 , CH_4 , C_2H_4) with low quantity of char used	75
Gasification	> 800	Air or H ₂ O vapour	Gas (H ₂ , CO, CO ₂ , CH ₄ , N ₂)	50-60
Liquefaction by Fast Pyrolysis	< 550	Low pressure	High viscosity liquid (phenols)	75
Direct liquefaction	300-350	CO high pressure	High viscosity liquid (phenols) non soluble in water	80



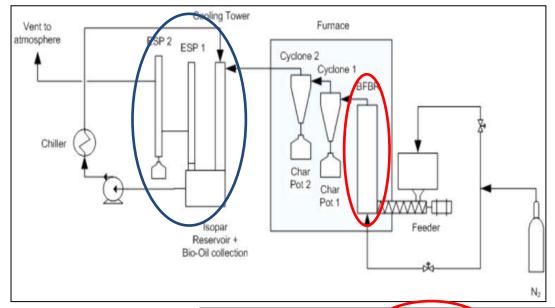
Pyrolysis, the key



Process	Temperature (°C)	Pressure (kPa)	Heating rate (°C min ⁻¹)	Residence time	Particle size	Atmosphere
Fast	450-600	101	100-300	2 s	2-5 mm	N ₂ or Ar
Slow	400-500	101	5-50	5-30 min	Large	N ₂ or Ar
Vacuum	350-500	10	5-50	2-30 s	large	Vacuum



Pyrolytic reactors

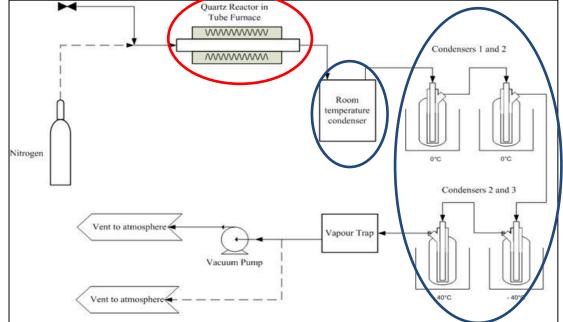


Fast pyrolysis

Bubbling Fluidized Bed reactor Electrostatic separator

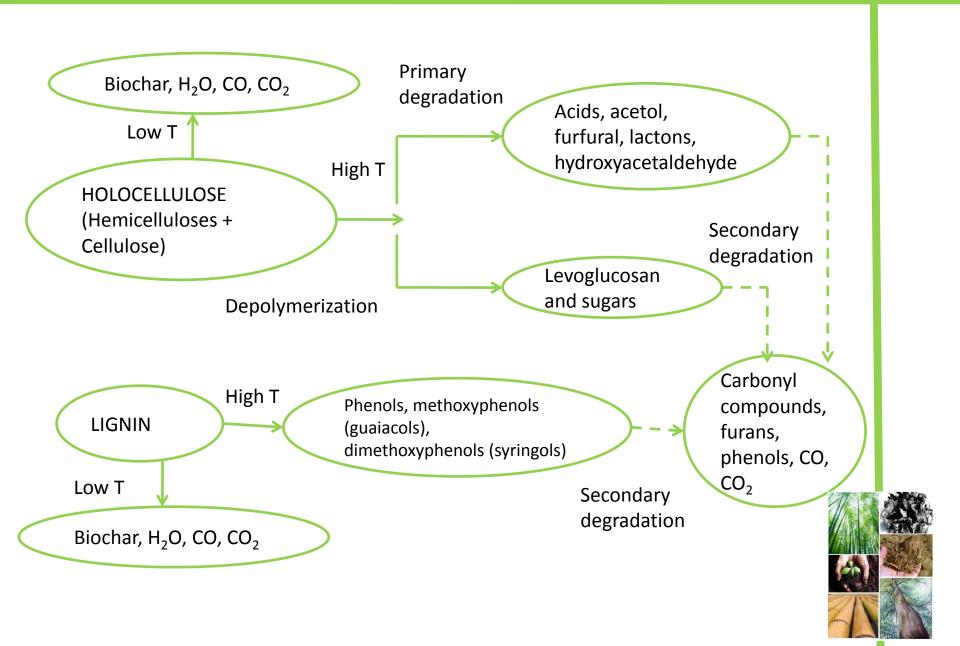
Slow/Vacuum pyrolysis

Fixed bed reactor
Series of condensers

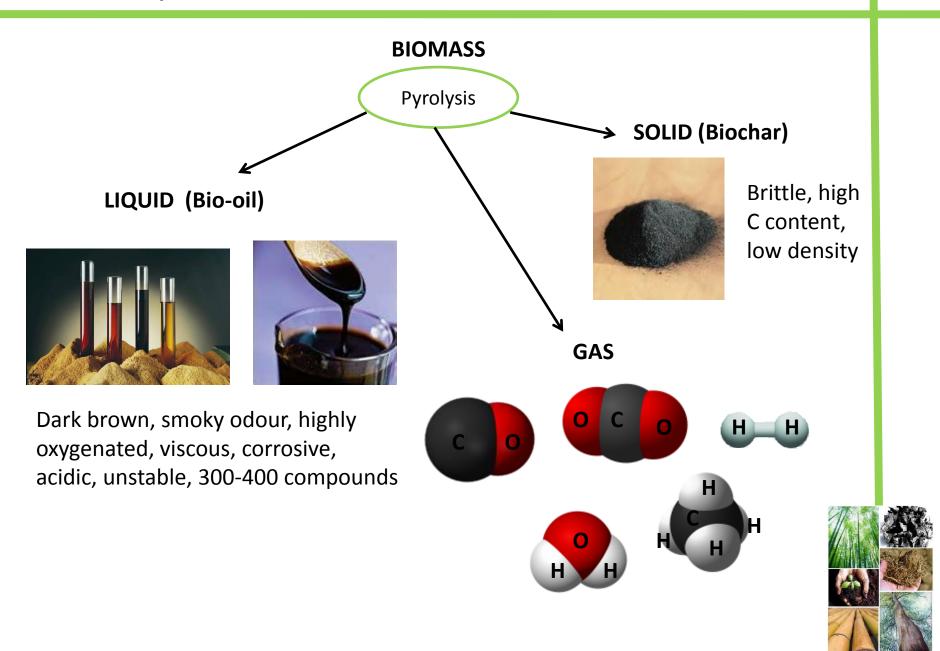




Mechanisms of degradation



Renewable products



Yields of renewable forestry products

Wood biomass	Process	YLiquid (wt.%)	YBiochar (wt.%)	YGas (wt.%)	Reference
100 % white wood	FP	70	18	12	Dynamotive, 2001
75/25 white wood/bark	FP	65	22	13	Dynamotive, 2001
50/50 white wood/bark	FP	63	23	14	Dynamotive, 2001
100 % bark	FP	58	27	15	Dynamotive, 2001
Eucalyptus	FP	76	13	11	Dynamotive, 2001
Eucalyptus	FP	71	25	9	Oasma, 2010
Eucalyptus	SP	46	38	16.0	Pimenta, 1998
Pine	FP	65-75	5-18	5-20	Wagenaar, 1993
Pine	SP	21-30	23-36	11-23	Sensoz, 2002
Black wattle	VP	27	38	35	Uras, 2010
Softwood bark	VP	23-28	57-57	15-21	Darmstadt, 2000

- Maximization of bio-oil yield for Fast Pyrolysis
- Influence of the feedstock nature
- Good distribution in product yields for Slow and Vacuum pyrolysis



Influence of parameters

Size of particles (SP)
Moisture content (MC)
Ash content (AC)

Temperature (T)
Pressure (P)
Heating rate (HR)
Residence time (RT)
Flow of nitrogen (FN)

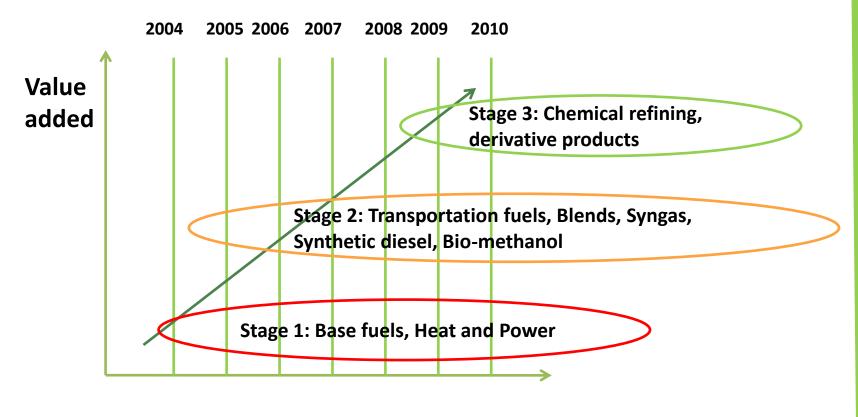
	SP	MC	AC	Т	Р	HR	RT	FN
	(µm)			(°C)	(kPa)	(°C min ⁻¹)		
Ybio-oil	< 450	Slightly /	High	500-900	(+)	Higher rate	Long time	(=/+)
	(-)	cont. (+)	cont. (-)	(-)		(+)	(=)	
HHV oil		Slightly /			10	Low rate	Long time	
		cont. (+)			(-)	(+)	(=)	
Ychar	2500	Slightly	High	500-900	(+)	Low rate	Long time	High flow
	(+)	influence	cont. (-)	(-)		(+)	(-)	(-)
HHV char			High	500-700	(-)	Low rate	Long time	High flow
			cont. (-)	(+)		(+)	(+)	(-)
BET surface			High	350-500	(-)	Optimal rate	Optimal	
area			cont. (-)	(+)		~10	time~2h	



Toxicity of renewable products

Product	Health-Environmental Impacts					
Bio-oil	- Presence of Polycyclic Aromatic Hydrocarbons (PAH)					
	- Mutagenecity tests (Salmonella strains) with slow and fast bio-oils: Slow					
	toxic					
	- Eutrophication test: Low fertilising effect.					
	- Ecotoxicologic effect: Acute toxicity of slow pyrolysis oil on Daphnia					
	- Corrosive, moderate sensitizer					
Biochar	Presence of heavy metals which are toxic					
Gases						
CO ₂ , CxHy	- Green House Gases contribution					
CO, H ₂ S, NOx	- Toxic gas emission					
HCl, HF, SO ₂	- Acidic rain					
Ash	- Serious health hazard, because the nano-particles are easily inhaled and					
	can cause lung damage.					



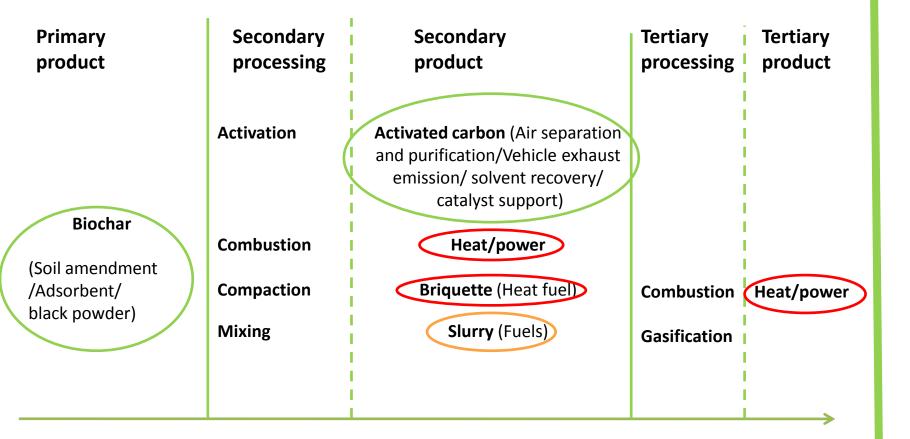


Time



Stage 1

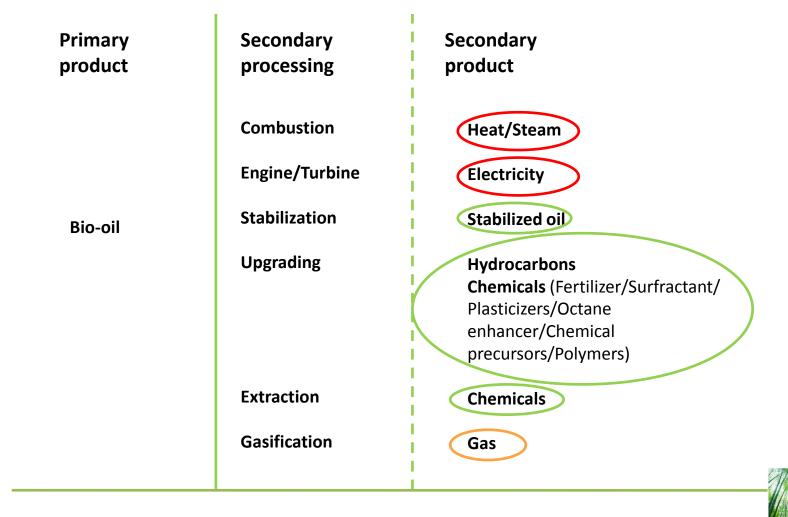
Stage 2





Stage 1

Stage 2



Stage 1

Stage 2

Primary product	Secondary processing	Secondary product	Tertiary processing	Tertiary product
Gas (Syngas/Hydrogen/ alkanes/ other hydrocarbons/ steam)	Fischer-Tropsch Combustion Engine/turbine	Liquid Fuel Heat/steam Electricity	Combustion	Electricity
Ash (Cement bricks/Road fill/Solidification of sludges/Soil amendment)	Fuel cell	Electricity		

Stage 1

Stage 2



Commercial plants

-Vacuum moving bed

-Rotating cone reactor

-Auger systems

??? 2010... 1990s-2010 Commercialization **Commissioning** 1980s-1990s of full scale pilot **Pilot plants Development of Biorefeneries** special reactors **New applications** other than -bioliq, KIT germany, 500 kg/hr biofuels (2009)-Union Fenosa, Spain 160 kg/hr - Dynamotive 200 t/day (2010) -Enel, Italy 650 kg/hr - IFP, France (2017) **Economic** -Wellman, UK -Envergent, US (2012) -Pyrovac, Canada -Entrained down-flow evaluation -Ensyn (2010) -Dynamotive, Canada 200 t/day -Ablative reactor -Fortum, Finland -Fluid bed -BTG, Netherland -Circulating fluid bed

-Ensyn, USA

-CRES, Greece

-Egemin, Belgium, 200 kg/hr

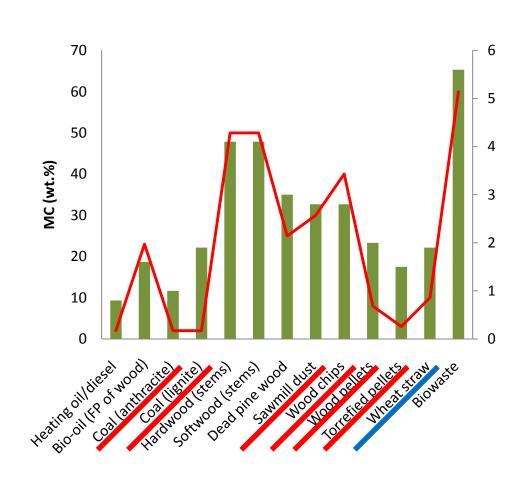


Keys-Challenges

- **Thermo-chemical processes more adapted** than bio-conversion to convert **wood** biomasses:
 - Wood contains a high lignin content which is not easily accessible for biological degradation
 - Ethanol production involves multiple steps (pretreatment, enzymatic or acid hydrolysis, fermentation and distillation.
 - 120 L aromatics/m³ = 180 L ethanol/m³
- Large choice of thermo-chemical processes for specific applications:
 - -Gasification for synthetic fuel and electricity production
 - -Liquefaction for chemicals and fuel production
 - -Slow/vacuum for biochar and activated carbon production
 - -Fast pyrolysis for fuel production
 - -Both, Chemical refining, derivative products
- **Transportation:** increase the energy density to decrease the cost of transportation



Transportation



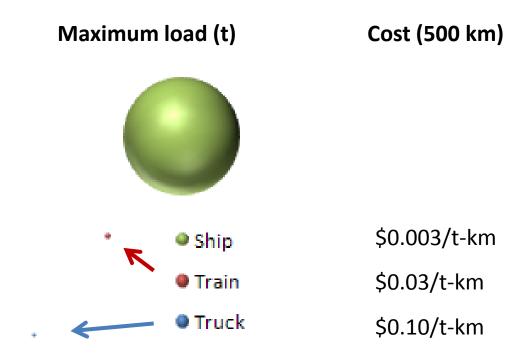


7.4 B-trains
2.5 B-trains

- Mass equivalent to the energy in 1 ton of coal (t)
- Moisture content (wt.%)



Transportation



Densification of wood:

- PELLETIZATION (Small portable pellet unit)
- TORREFACTION (Small portable pyrolysis unit)



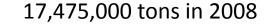
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- Potential of CO₂ sequestration



CO₂ sequestration





1,939,090 t CO₂ sequestered
 364,157,200 t CO₂ emissions for SA in 2003



Pyrolysis



Bio-oil + Gas

Combustion



Biochar

Soil amendment

Fast pyrolysis and slow pyrolysis, 10 wt.% and 27 wt.% of CO₂ sequestered, respectively

20 wt.% of raw forest wastes - 0.3 wt.% of reduction of CO₂ emissions



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- **Transportation:** increase the energy density to decrease the cost of transportation
- Potential of CO₂ sequestration
- Intensification of non-friendly environmental woody culture leading to the **soil impoverishment**



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Thank you for your attention

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